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# Separation of H<sub>2</sub> from natural gas-H<sub>2</sub> -mixtures

The H<sub>2</sub>-Membrane project

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### **ONTRAS Gastransport GmbH**



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### Feed-in from Power-to-Gas Facilities into the network of ONTRAS

#### Hybridkraftwerk Prenzlau

- Operated by ENERTRAG AG
- Power connection: 500 kWel
- $H_2$ -production: 120 m<sup>3</sup>/h
- Blending with natural gas in the ONTRAS system

### WindGas Falkenhagen

- Operated Uniper SE
- Power connection : 2.000 kWel
- H<sub>2</sub>-Production: 360 m<sup>3</sup>/h
- Additional methanation in operation since 2018



### **Background and motivation**

- Power-to-Gas uses the existing natural gas infrastructure
- We see a parallel development dedicated pipeline and H<sub>2</sub>-blending
  - Options for a coexistence of natural gas and hydrogen necessary
- Limitations for H<sub>2</sub> on the demand side of the natural gas infrastructure
  - CNG-filling stations: < 2 mol-%
  - Existing gas turbines: varying (between 1 4 mol-%)
  - Industrial applications: limits are under discussion, but steady H<sub>2</sub>-concentration is aspired
- Necessity of H<sub>2</sub>/natural gas mixtures
  - 10 mol-% H<sub>2</sub> in the natural gas grid in Germany permitted, higher limits in discussion
  - > 20 mol-%  $H_2$  potential future limit with replacements of application technology







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### Need for H<sub>2</sub>-treatment on pore storage facilities

#### **Gas storages**

- Caverns and pore storage facilities largely in use in Europe
- 75 % of the storages in Europe are pore storages
- In Germany most of the storage capacity in caverns
- On the long run, we need all the useful storage capacity for H<sub>2</sub>
- When you convert a natural gas storage, you will have H<sub>2</sub>/natural gas mixtures with variable composition over years

### **Treatment of the H<sub>2</sub>/natural gas mixture necessary**





### Separation technologies hydrogen/natural gas - Overview

#### **Membranes**

- Various materials (polymer, inorganic or palladiummembranes) under investigation in a laboratory scale
- Different materials are suitable
- For the specific use H<sub>2</sub>/natural gas no facility in in operational environment

#### **Chemical transformation**

- **Catalytic methanation of H**<sub>2</sub> Alternative for protection of facilities
- **Oxidation** chemical reaction of  $H_2$  with oxygen into water feasible, but  $H_2$  is annihilated

#### **Adsorption**

- Under given conditions an adsorption of H<sub>2</sub> not feasible
- adsorptive separation is economically relevant in concentrations from 50 % H<sub>2</sub> and higher

#### **Miscellaneous**

• Cryogen H<sub>2</sub>-separation technically feasible

Membrane techniques, methanation and oxidation basically feasible

More details see DVGW R&D project: Anforderungen, Möglichkeiten und Grenzen der Abtrennung von Wasserstoff aus Wasserstoff/Erdgasgemischen (G 201611)

### Advantages of membrane techniques

- Little complexity
- Low OPEX
  - Main "feed stock" pressure available in gas networks
  - Works mostly under ambient temperature conditions
- Flexibility
- No by-products (disposal of waste)
- No chemicals necessary
- Different materials available (R&D)
- Compactness



### Surrounding conditions for membrane techniques

- For facilities with a smaller scale the costs for the membranes are secondary (mainly costs for installations)
- Costs depend on different conditions (pressure, number membrane stages, desulphurization...)
- OPEX are dominated by compressor usage
- $H_2$  purity > 99,9 % possible with Pd-membranes; other membranes 96 98 %
- More details to costs, see DVGW R&D project DVGW G 201611

- Existing ONTRAS-Feed-in facility for Hydrogen
- Pressure: max. 25 bar
- Hydrogen concentration variable from 0 to 50 Vol.-%, fixed rate in every experimental run
- Volume flow from 1 to 2 m<sup>3</sup> mixture per hour



#### **Partners**

- DBI Gas- und Umwelttechnik GmbH
- ONTRAS Gastransport GmbH
- GRTgaz S.A. Forschungszentrum RICE, France
- Mitteldeutsche Netzgesellschaft Gas mbH
- DVGW Deutscher Verein des Gas- und Wasserfaches e.V.
- Associate partner: ENERTRAG AG





Source: Fraunhofer IKTS







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- Online monitoring of gas quality by using gas chromatography
- Remote supervision and control by DBI from Leipzig



### **Test strategy**

Membrane types	Status quo
Polymer membrane	Membranes in testing
Inorganic membranes	Membranes at hand / in preliminary investigation in the laboratory
Inorganic membranes (molecular sieve)	Membranes at hand / in preliminary investigation in the laboratory
Pd-membranes	Matching of test conditions with the manufacturer

### Test procedure

	Desciption	Duration in days	Conditions
1	Polymer membrane number 1	3	H₂/NG 10/90 Pressure ca. 20 bar
2		2	H₂/NG 10/90 Pressure ca. 10 bar
3		2	H <sub>2</sub> /NG 20/80 Pressure ca. 20 bar
4		2	H₂/NG 20/80 Pressure ca. 10 bar
5	Stability test: replication of test number 1	2	H₂/NG 10/90 Pressure ca. 20 bar
6	Simulation of a second membrane stage	3	H <sub>2</sub> /NG 50/50 Pressure ca. 20 bar

### First results

### Accelerated test in Prenzlau

- Polymer membrane with an mixture of  $H_2/NG$  10/90
  - $H_2 > 40$  mol-% in permeate, second stage necessary for higher purity

### New results from the laboratory tests

With carbon membranes hydrogen level can be raised from 98 mol-% (DVGW G 260 : Group A) to 99,97 mol-% (Gruppe D) → seems to be feasible

### **General remarks**

 Pd-Membranes are able to extract very pure hydrogen (> 99,97 – mol-%) under stable conditions (tests in Spain)

Thank you very much for your attention, please feel free to ask your questions!

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